

EAST Search History

Ref #	Hits	Search Query	DBs	Default Operator	Plurals	Time Stamp
S1	1	hydrocarbon with (distillation adj3 column)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:17
S2	2831	hydrocarbon with (distillation adj3 column)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S3	103	hydrocarbon adj distillation adj3 column	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:19
S4	97	hydrocarbon adj distillation adj column	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S5	4	S4 and simulation	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S6	341	(hydrocarbon with (distillation adj3 column)) and simulat\$4	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:27
S7	19	(hydrocarbon with (distillation adj3 column)) same simulat\$4	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:23
S8	0	S6 and lumping	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:23

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S9	41	S6 and lump\$5	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:26
S10	15	(lumping adj3 method)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:26
S11	181	S6 not S9	USPAT	OR	OFF	2006/10/26 11:27
S12	4	S11 and constituents and (material with balance)	USPAT	OR	ON	2006/10/26 11:28

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[**Simulation of Compositional Processes: The Use of Pseudocomponents in Equation-of-State Calculations**](#)

SPE eLibrary The accuracy of the method is demonstrated by comparing phase splits, lumped mole fractions in liquid and vapor phases, and phase densities and phase viscosities obtained from a lumped fluid description with the same data as those obtained from a fully compositional description of hydrocarbon systems. Let us now consider a lumped description of then \sim component system in terms of n groups, numbered S , t , 11 i., To handle the minimization problem, we choose as variables the liquid mole numbers, $n_p, h = x_p s_f L, s = 1$.

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[**Reliable Wax Predictions for Flow Assurance**](#)

SPE eLibrary The recently developed model of Coutinho is, however, based on high accuracy thermodynamic data. In order to put wax calculations on a firmer footing, Coutinho and co-workers have developed a wax model that is directly based on high-quality laboratory data for the properties of liquid and solid hydrocarbons and their mixtures [9,10] We believe that this behaviour is an artifact of the lumped model. Lumping the non- n -paraffins has virtually no effect on the wax calculations.

89%



[**Prediction of CO₂/Crude Oil Phase Behavior Using Supercritical Fluid Chromatography**](#)

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[Obtaining PVT Data For Very Sour Retrograde Condensate Gas and Volatile Oil Reservoirs: A Multi-disciplinary Approach](#)

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Finally, to obtain good matches on liquid densities, volume shifts on the heavier components was the third targeted tuning factor(s). This was done by assigning properties to the heaviest component which corresponded to progressively higher molecular weight pseudo components. Most of the lumping schemes suggested for developing pseudo components usually pick a carbon number that is closer to the smaller end of the range. Therefore, the second or third lowest carbon number component in a pseudo component range, is usually considered the best average.

82%



[Simulation of Gas Condensate Reservoir Performance](#)

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This paper presents a pseudoization procedure that reduces the multicomponent condensate fluid to a pseudo two-component mixture of surface gas and oil. We can think of pseudoization in terms of either lumping components or combining streams. The mixture might be flashed at a low pressure and temperature with liquid and gas separator products resulting. In lumping components, each pseudocomponent consists of a subset of the original n components, and none of the members of this subset are present in any of the other pseudocomponents.

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[Predicting Retrograde Phenomena and Miscibility Using Equation of State](#)

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condensation and condensing-gas-drive recovery to achieve dynamic miscible displacement or multiple phenomena have important applications in NGL production and contact miscible displacement. In Table I the mixing rules for these parameters are based on different conformal solution theories of mixtures. An equation of state, such as Equation 1 with a choice of mixing rules is based on binary interactions. The parameters A_{ij} , b_{ij} , and C_{ij} of this equation of state are derived from pure component properties while parameters A_{ij} , b_{ij} and C_{ij} are derived from binary data of i and j .

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